

Correction to *P*, ρ , *T* Measurements and Isobaric Vapor–Liquid Equilibria of the 1,3,3-Trimethyl-2-oxabicyclo[2,2,2]octane + Propan-1-ol Mixture: Cubic and Statistical Associating Fluid Theory-Based Equation of State Analysis [*Journal of Chemical & Engineering Data* 2010, 55, 5932–5940 DOI: 10.1021/jc100577v]. Marcos Torcal, Sandra García-Abarrio, Juan I. Pardo,* Ana M. Mainar, and José S. Urieta

In the original document (*J. Chem. Eng. Data* 2010, 55 (12), 5932–5940), page 5937, Table 7 and page 5938, Table 9 contained errors in the data concerning 1,8-cineole. The corrected data are reported.

Table 7. Coefficients for the Equations of Vapor Pressure. The Equation of Antoine Provides P^{sat} /kPa Using T /K. Capital Letters: Equation of Antoine; Lower Case Letters: Wagner Equation

	<i>A/a</i>	<i>B/b</i>	<i>C/c</i>	<i>d</i>	T_{min}/K	T_{max}/K
1,8-cineole	13.9128	3523.60	−70.03		326.65	449.15
1-propanol ^a	−8.53706	1.96214	−7.6918	2.945		T_c^a

^aRef 14.

Table 9. Properties and Parameters of the Pure Components Used for the Application of the EOS

PR and PT	T_c/K		P_c/MPa		ω	
1,8-cineole	661.12 ^a		3.019 ^d		0.338 ^b	
propan-1-ol	536.98 ^c		5.175 ^c		0.629 ^c	
SAFT	<i>m</i>	$v^{\text{oo}}/\text{L}\cdot\text{mol}^{-1}$	$u^0/\text{k}/\text{K}$	κ	$\epsilon/\text{k}/\text{K}$	range T/K
1,8-cineole	5.2966	0.015698	250.71	0	0	326.65–449.15
propan-1-ol	3.240 ^d	0.0120 ^d	225.68 ^d	0.01968 ^d	2619 ^d	293–493 ^d
PC-SAFT	m_i	$\sigma_i/\text{Å}$	$\epsilon_i/\text{k}/\text{K}$	k^{A,B_i}	$\epsilon^{A,B_i}/\text{k}/\text{K}$	range T/K
1,8-cineole	3.4254	4.0597	291.37	0	0	326.65–449.15
propan-1-ol	2.9997 ^e	3.2522 ^e	233.40 ^e	0.015268 ^e	2276.8 ^e	240–537 ^e

^aJoback's method, ref 35. ^bLee–Kesler method, ref 36. ^cRef 13. ^dRef 38. ^eRef 42.

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